

Commercial Systems Treating both High and Low Strength Perchlorate Applications Utilizing Ion Exchange

By

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Agenda

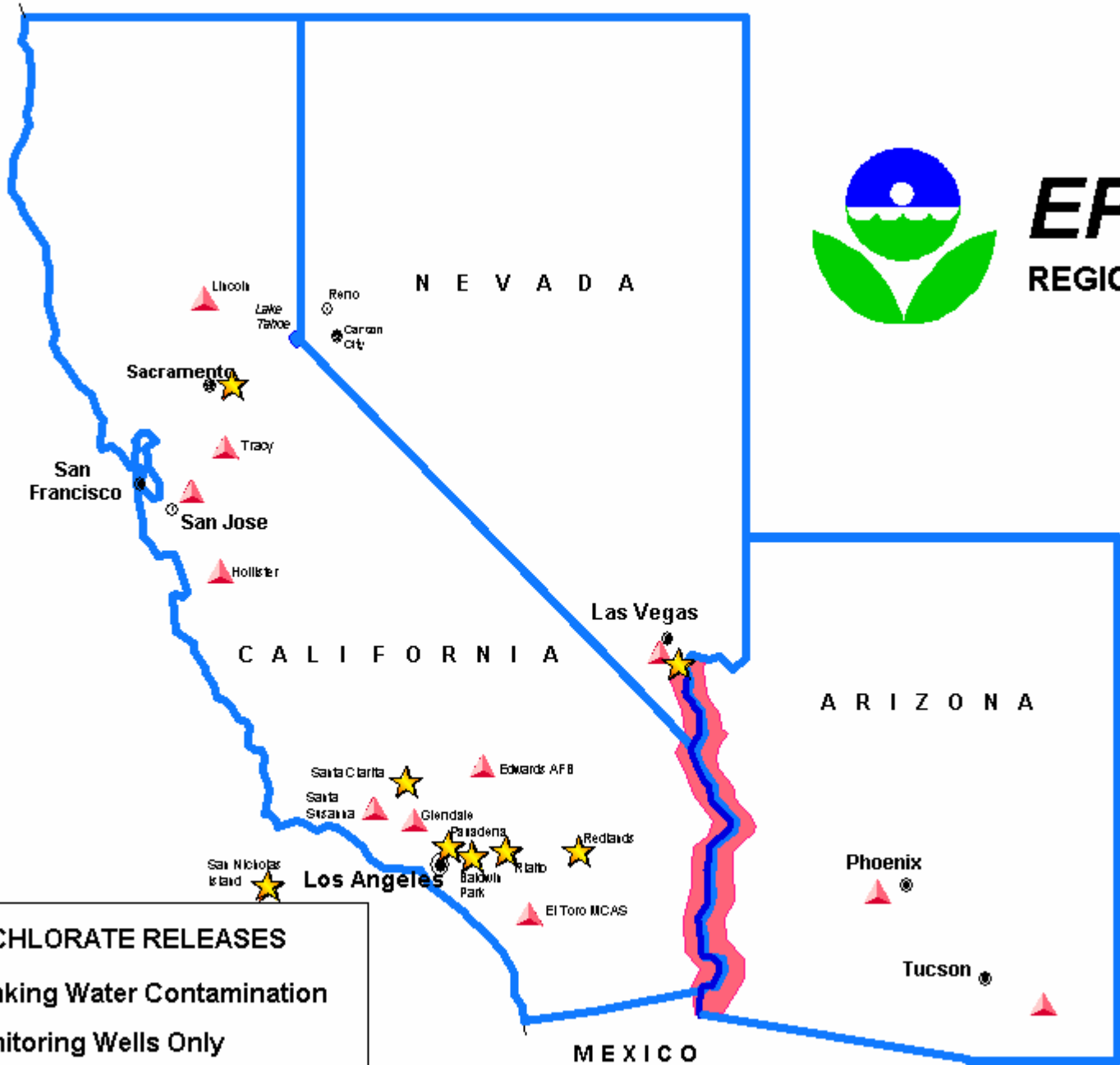
- IX Development Chronology
- ISEP & ISEP+ Systems
- Pilot Tests
- Operating Systems
 - High Strength Application
 - Low Strength Application

ISEP & ISEP+ Systems

- 1/98 – CCC conducted first lab tests
- 8/98 – Completed first successful field pilot tests
 - San Gabriel Valley, CA
- 1/99 – Completed perchlorate removal and destruction pilot tests
 - NASA's Jet Propulsion Lab – Pasadena, CA
- 11/99 – First remediation system
 - Henderson, NV
- 2/00 – First potable water system
 - LaPuente, CA



EPA
REGION 9



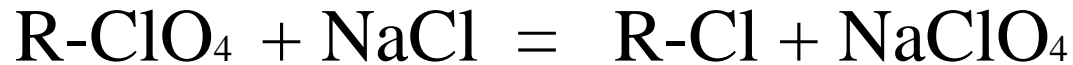
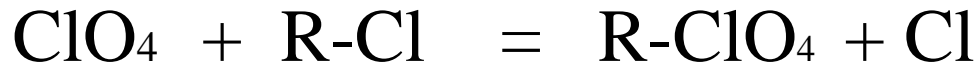
PERCHLORATE RELEASES

- ★ Drinking Water Contamination
- ▲ Monitoring Wells Only
- Colorado River Contamination

June, 1999

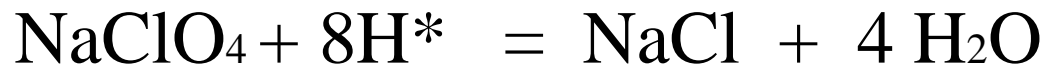
Ion Exchange Process

- Removal/Regeneration – IX resin



(R) – IX resin

- Destruction – Catalytic Reduction

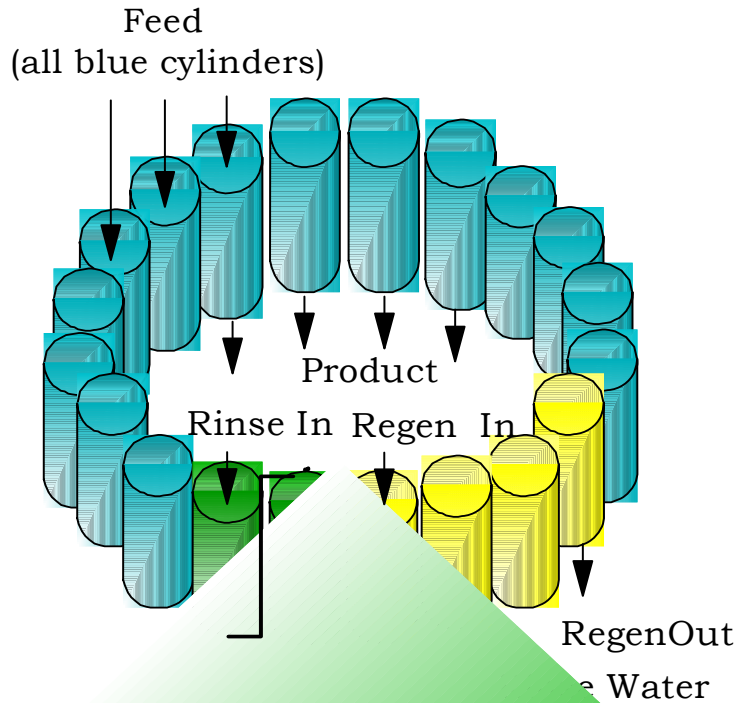


(H*) – hydrogen source

ISEP & ISEP Systems

- ISEP System – Continuous ion exchange process to remove perchlorate and nitrate from water
- ISEP+ System – Continuous ion exchange process to remove and **destroy** perchlorate and nitrate from water

ISEP Illustration

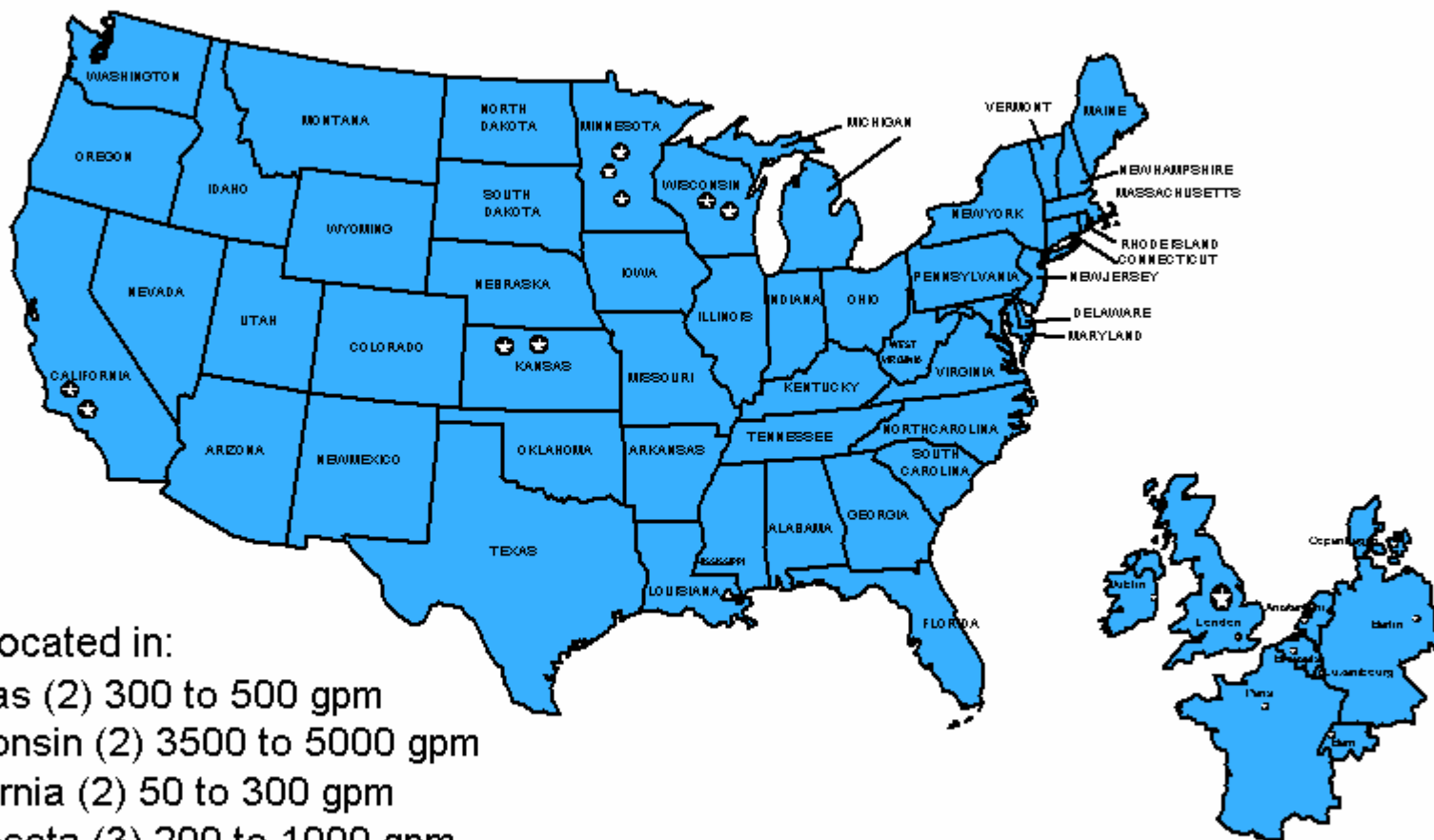


ISEP Design Features

- ▶ Configuration flexibility
- ▶ Reduced resin inventory
- ▶ Simplified control philosophy
- ▶ Reduced regeneration chemicals
- ▶ Steady state operation

Calgon Carbon ISEP Experience

Drinking Water Plants



- Plants located in:
 - ▶ Kansas (2) 300 to 500 gpm
 - ▶ Wisconsin (2) 3500 to 5000 gpm
 - ▶ California (2) 50 to 300 gpm
 - ▶ Minnesota (3) 200 to 1000 gpm
 - ▶ United Kingdom (1) 1000 gpm

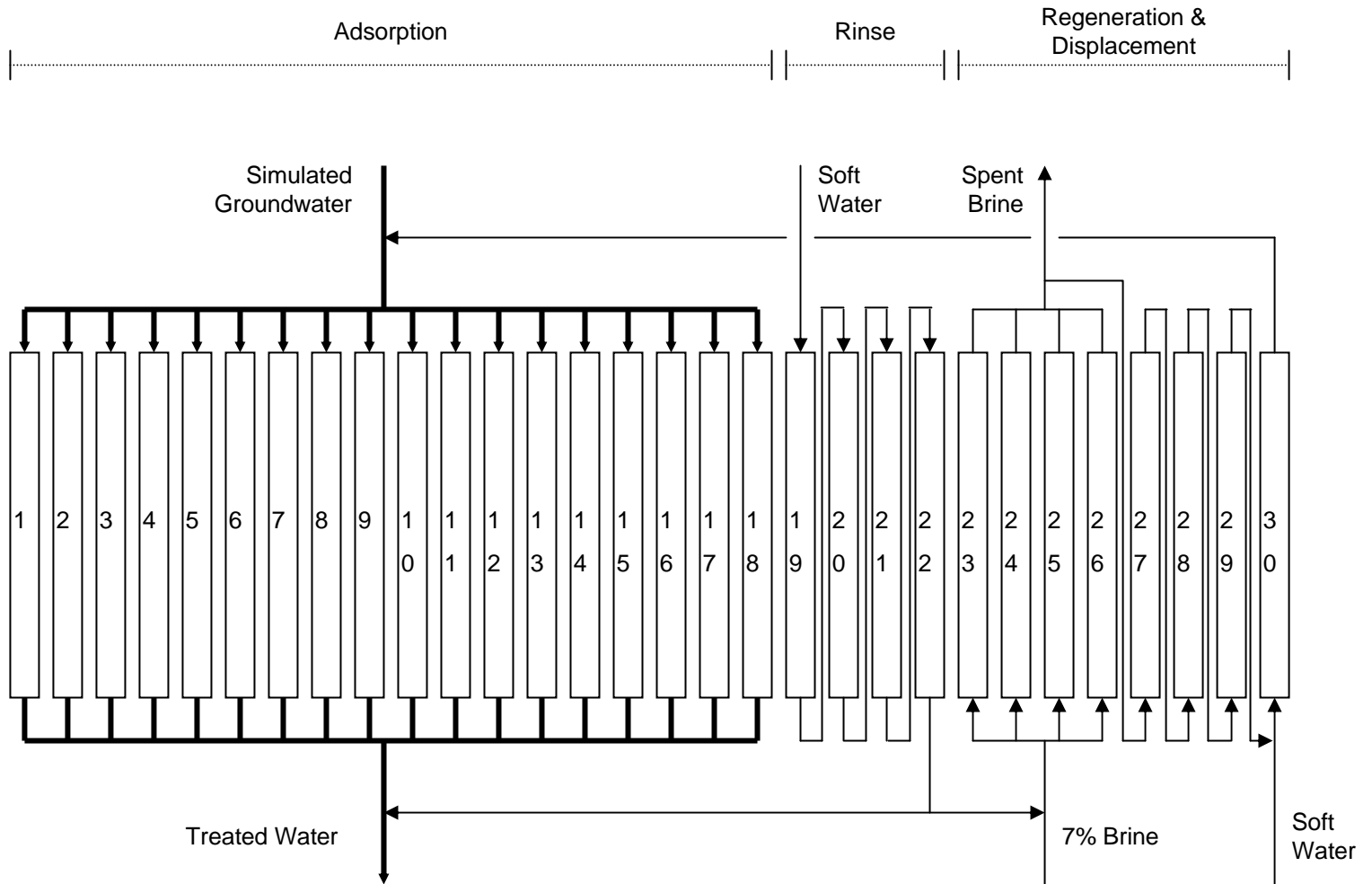


Figure 1. Schematic of the ISEP® Ion Exchange Process

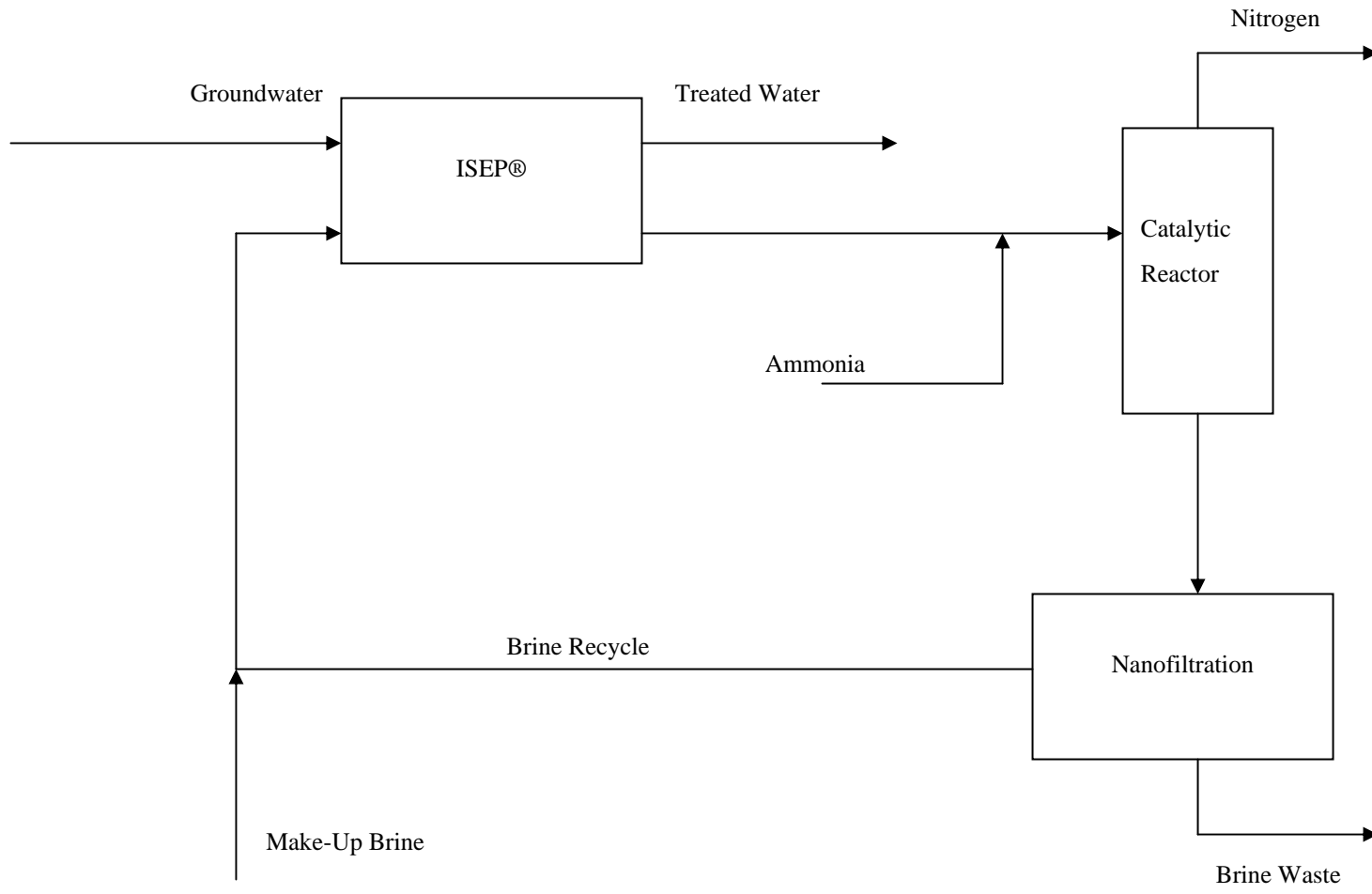
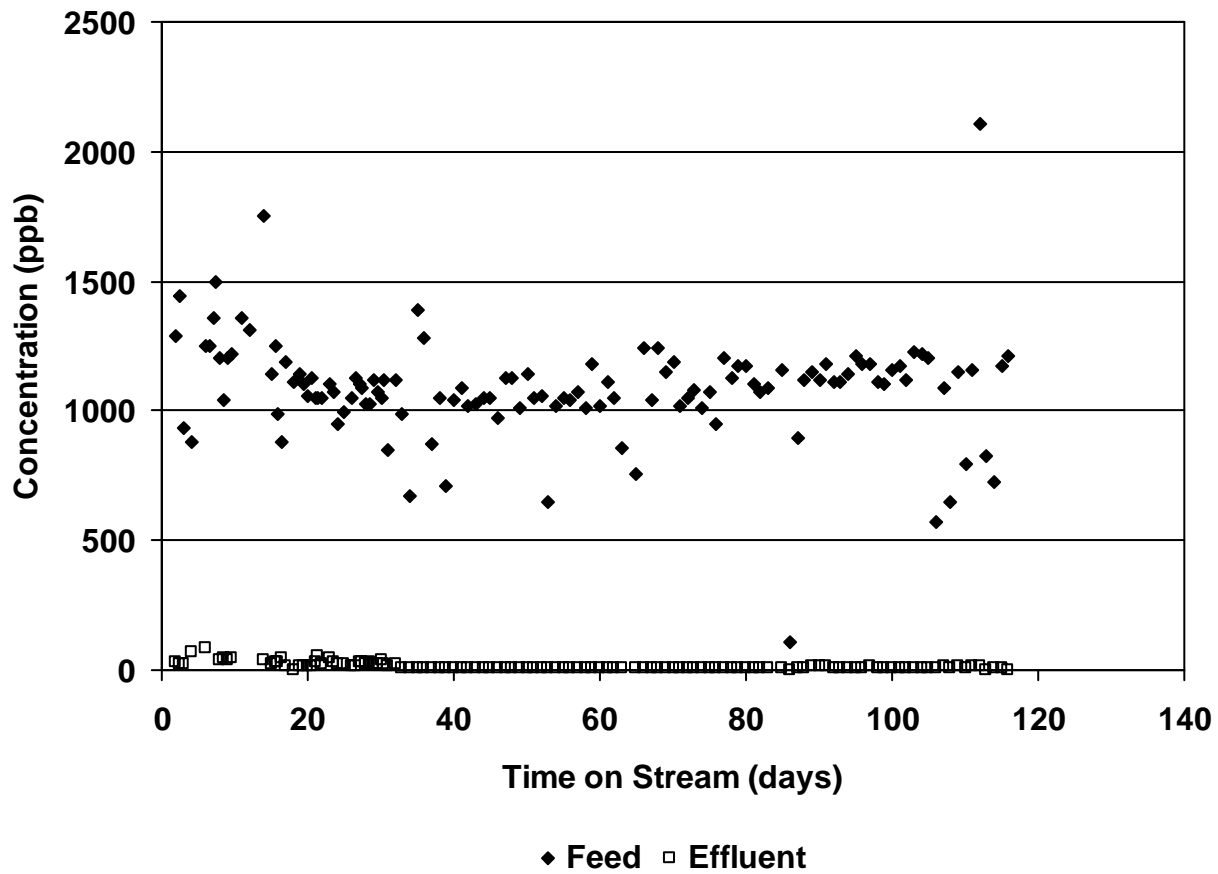
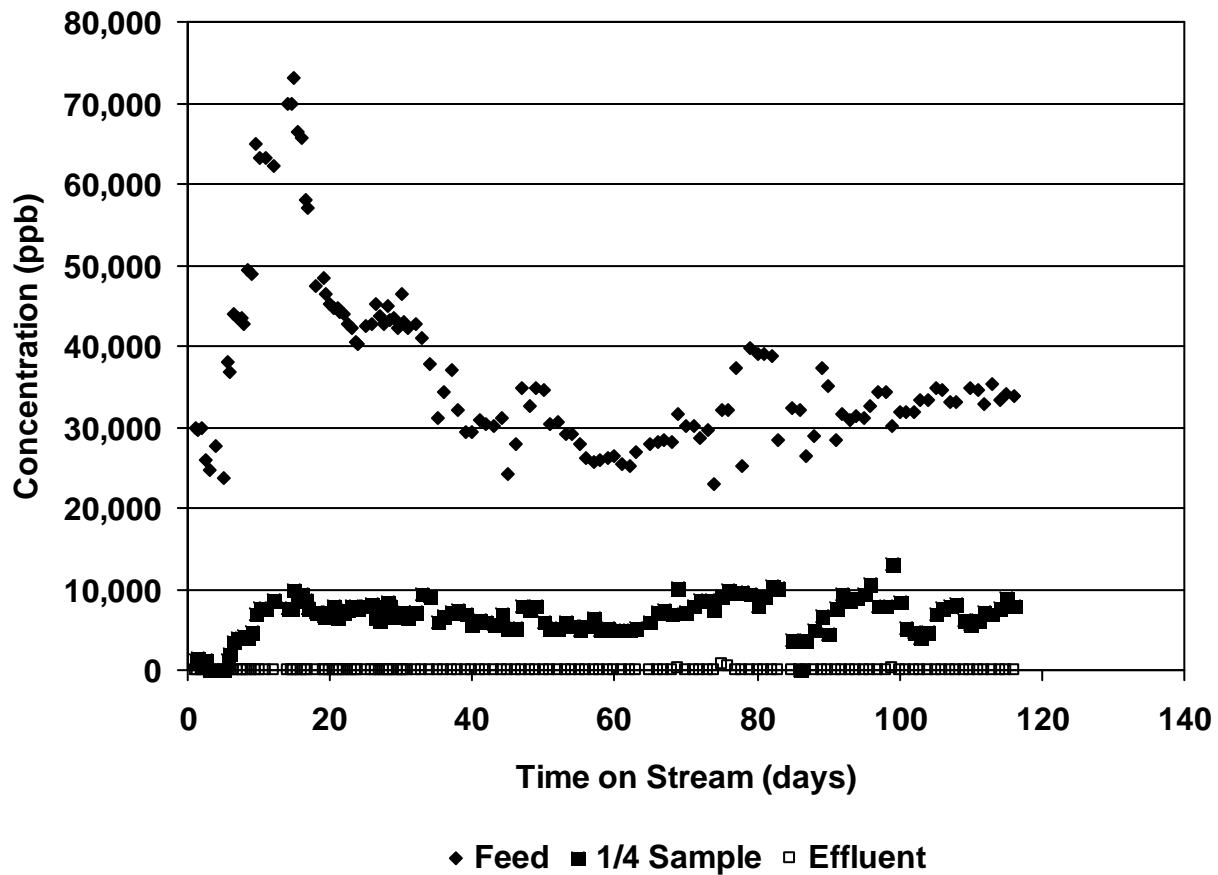


Figure 2. Block-Flow Diagram of the ISEP+™ Process



Non-Detectable ClO_4^- Levels Recorded as 4 ppb

Figure 3. Perchlorate Removal in the ISEP®



Non-Detectable ClO_4^- Levels Recorded as 100 ppb

Figure 4. Destruction of Perchlorate in the Reactor

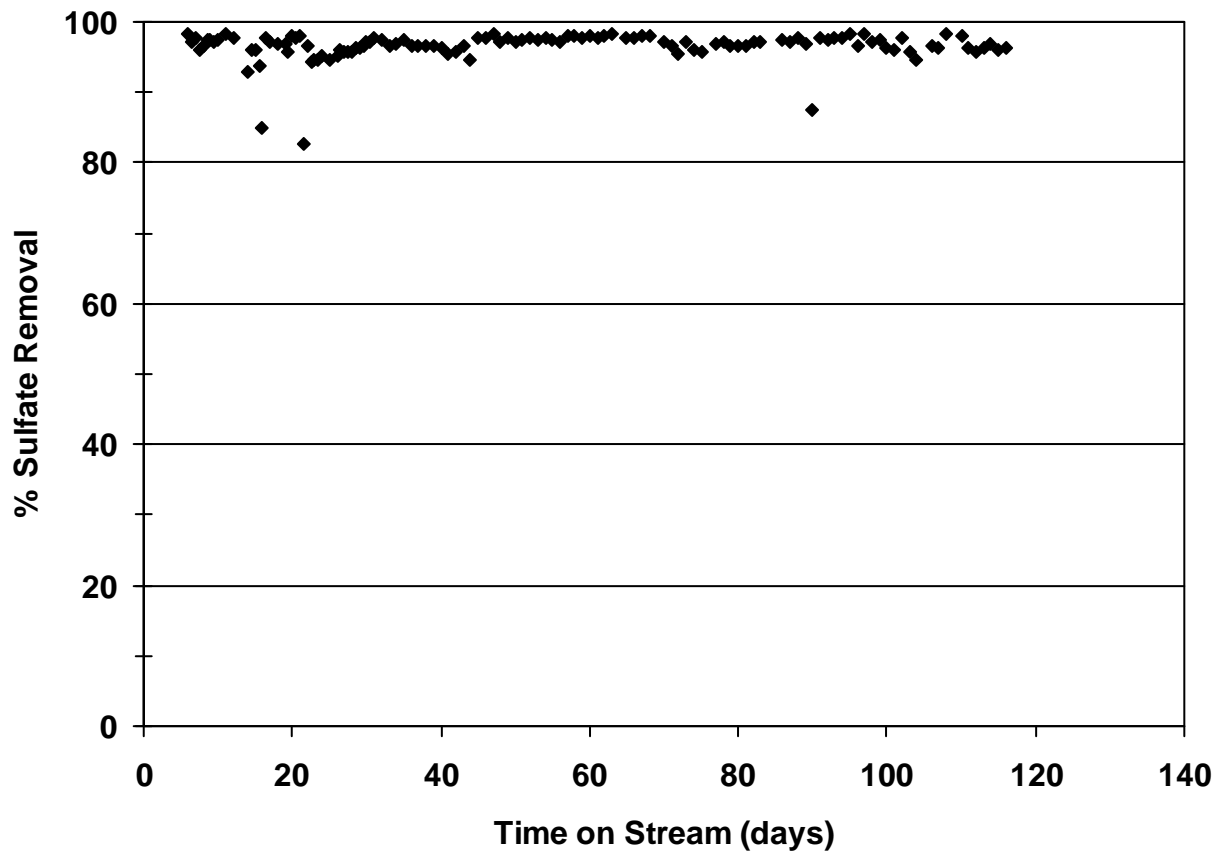


Figure 5. Sulfate Removal in the Nanofiltration Process

Henderson, NV Remediation

- Remediation application
- Instillation designed to treat perchlorate containing seep water draining into Lake Mead
- System was commissioned in November 1999 and has been in continuous operation since that time

Henderson, NV Remediation

- Ion exchange system is designed to remove 100 ppm of perchlorate
 - Actual levels have varied from 80 – 110 ppm
- System designed to treat 450 gpm of water
 - Flow rates have varied from 200 – 560 gpm
- System designed to achieve 97 % perchlorate removal
 - Typical effluent perchlorate effluent levels are non detectable on an ion selective electrode (<2 ppm)

La Puente Valley County Water District ISEP System

- 2500 gpm drinking water application
- Designed to treat perchlorate, volatile organics, NDMA, and 1,4-dioxane
- System was commissioned in February 2000

La Puente Valley County Water District

- ISEP System accepted by CADHS for perchlorate and nitrate drinking water applications
- Operating permit currently under review by CADHS – Metropolitan District
- Emergency use permit approved
- Currently ISEP system is operating 19 hr/day to control perchlorate plume

Capital Costs

- Estimated Capital January 1999
- \$4,600,000
- Actual Capital 03/31/00
- \$4,070,041
- Engineering and permits for DOHS Testing
- \$882,608 (Budgeted \$314,399)
- Total \$4,952,649
- Overrun \$352,649

La Puente Operational Costs

	Budget 1/99	Actual
Wells*	\$21/AF	\$21/AF
Air Strippers	\$7/AF	\$7/AF
Booster	\$7/AF	\$7/AF
ISEP	\$69.98/AF	\$52.34/AF
Brine Disp.	\$21/AF	\$4/AF
Rayox	\$89.72/AF	\$42.61/AF
Peroxide	\$16.32/AF	\$7/AF
Maint/Labor	\$59.18/AF	\$86.71/AF
Total	\$291.20/AF	\$227.66/AF
Savings		\$63.54/AF





Summary

- ISEP Systems capable of treating both high and low strength perchlorate applications at very low waste brine levels
- ISEP+ Systems capable of treating and destroying perchlorate at very low or zero waste levels